

考試科目：反應工程

研究所
 大學部
 工程在職進修

系班別：

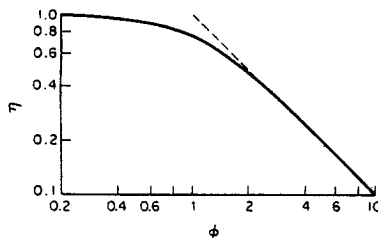
閉書式考卷

一. 有一個 first-order irreversible reaction $A(g) \rightarrow B(g)$ 在一個半徑為 0.5 cm 的孔 + 壁筒內 (15%) 進行。假設 effective diffusivity $D_e = 0.014\text{ cm}^2/\text{s}$, activation energy $E = 25\text{ kcal/mol}$, reaction rate constant $k_1 S_0 P_0 = 0.8\text{ s}^{-1}$ at 100°C , 反應是在 1 atm , 100°C 下進行, 假設無 film mass transfer resistance, 請問

(i) 此時的 overall real reaction rate $(-r_A)$ 為多少 g-mole/s-l ?

(ii) 此時是何種 control region, 你怎麼看出來的?

$$R = 82.05 \frac{\text{cm}^3 \cdot \text{atm}}{\text{g-mole} \cdot \text{K}}$$

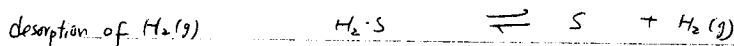
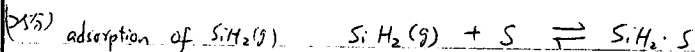


Sphere $\phi = (R/3)\sqrt{k_1 S_0 P_0 / D_e}$

Cylinder $\phi = (R/2)\sqrt{k_1 S_0 P_0 / D_e}$

Slab $\phi = L\sqrt{k_1 S_0 P_0 / D_e}$

二. SiH_2 氣體 deposit 在 substrate 上 - 層 $\text{Si}(s)$ film 的 mechanism 是 (25%)



如果 surface reaction 非常慢而 control 了 overall reaction 時, 請導出 overall silicon deposition rate R_{Si} 的 expression. 假設

P_{SiH_2} = SiH_2 的 partial pressure

P_{H_2} = H_2 的 partial pressure

f_v = vacant site 所占的 fraction

f_{SiH_2} = 被 SiH_2 adsorbed site 所占的 fraction

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三. 有一個容器不斷的有 solvent 流進及流出, 呈 steady state 狀態。如果在 $t=0$ 時在進口外打 (15%) 了 50 g/m^3 的 tracer, 以 pulse 的方式打入。在出口外, 我們量到的 tracer concentration 與時間關係為

$t(\text{min})$	0	1	2	3	4	5	6	7	8	9	10	12	14
$C(\text{g/m}^3)$	0	1	5	8.2	10.2	8.2	6.2	4.2	3.0	2.2	1.5	0.6	0

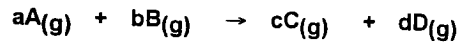
請給出它的

(i) C curve

(ii) E curve

(4) Please derive a mole balance equation on species j and make some assumptions to obtain design equations for (a) Batch Reactor (b) CSTR and (c) Plug-Flow Reactor. (15%)

(5) Please write down the stoichiometric table for a continuous-flow reactor. The reaction can be expressed as



Please take A as the basis and express the concentration of A in conversion. (15%)

(6) A reaction takes place in a batch reactor. The reactor volume is 20 liter. The rate expression can be expressed as

$$-r_A = kC_A \quad (k = 0.02 \text{ min}^{-1})$$

Please calculate the time t necessary to achieve a conversion of 0.8 ($X_A = 0.8$). (20%)